

Original Research Article

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Bioethanol Production from Cotton Stalk Hydrolysate using Immobilized Co culture of *Saccharomyces cerevisiae* and *Pachysoletannophilus*

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ABSTRACT

Keywords

Fermentation, Bioethanol, Cotton stalk, *Saccharomyces cerevisiae*, *Pachysoletannophilus*, Immobilization.

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The present study focuses on bioethanol production from cotton stalk hydrolysate using immobilized cell fermentation. For this, cotton stalk was hydrolyzed by two stage acid treatment, and the obtained hydrolysate was detoxified and fermented using immobilized co culture of *Saccharomyces cerevisiae* MTCC36 and *Pachysoletannophilus* MTCC1077. The results showed that, maximum ethanol concentration of 3.94 g/L was achieved after 36 hours of fermentation by consuming 90.18% of total available sugar, with a corresponding yield of 0.142 g/g biomass, 0.221 g/g of holocelluloses, 0.355 g/g of fermentable sugar, and fermentation efficiency of 69.53% respectively. As recycling of immobilized cell is concern, the first two batches gave significantly similar results in concentration, yield and fermentation efficiency, while during third cycle of fermentation, beads became disintegrated.

Introduction

Increasing energy demand and decreasing fossil reservoirs, diverts the concentration of research towards an alternative energy sources. These energy sources must be expected to satisfy several requirements, including substantial reduction in greenhouse gasses emission, world wide availability of feedstock and capability of being produce from renewable resources. Many alternative fuel sources have been explored and among them fuel ethanol have received most attention. Ethanol is renewable energy source produced through fermentation of sugar. As a substrate, conventional crop such as corn and sugarcane are unable to meet the global

demand of bioethanol production due to their primary value of food and feed therefore, lignocellulosic substance such as agricultural wastes are emerged as attractive feedstock for bioethanol production (Dien *et al.*, 1999). In present study cotton stalk was used as feedstock due to its lignocellulosic nature and potential availability.

Before going to ethanol fermentation, the feedstock needs to be process by scarification technology in order to retain fermentable sugars. Acid hydrolysis is a simple and easy method to perform and is prominently used for depolymerization of biomass into fermentable sugar. Acid

hydrolysis was carried out in two stages including concentrated acid decrystallization followed by dilute acid hydrolysis with steam and heat treatment (Liao *et al.*, 2006). As soon as the monomers are produced, further decompositions occur, yielding other unexpected compounds such as furans and phenolics; which negatively impact on fermentation process. To overcome these inhibitors, detoxification of acid hydrolysate was the next key step in series before fermentation (Chandel *et al.*, 2007).

The use of immobilized cell offers number of advantages such as enhancement of fermentation productivity, feasibility of continuous processing, cell stability, lower costs of recovery and recycling in downstream processing (Kourkoutas *et al.*, 2004). Cell entrapment using calcium alginate gel is a well-established technique which has been extensively studied because of its simplicity and non-toxicity. Alginic acid is natural polymer found in marine algae (Davis *et al.*, 2003). The fact that free carboxylic groups are repeated in the macromolecule makes them accessible to divalent cations such as Ca^{2+} , and formation of coordination complexes occurs in gelation process (Vullo and Wachsmann, 2005). The preparation process is known as electrostatic droplet generation method, which is carried out by drop-wise addition of cell suspended in sodium alginate in to the calcium chloride solution, where beads are immediately formed in the calcium alginate gel (Goksungur and Zorlu, 2001).

Immobilization of cells for fermentation has developed to eliminate inhibition caused by high concentration of substrate and products, also to enhance the productivity and yield of ethanol production (Baptista *et al.*, 2006). In present study, co culture of *Saccharomyces cerevisiae* and *Pachysolen tannophilus* were

immobilized in calcium alginate beads and evaluate its potential for ethanol production using cotton stalk hydrolysate as sole carbon source.

Materials and Methods

Feed stock preparation

Cotton stalks of spp. *Gossypium hirsutum* NHH44 was collected, dried, debarked, and ground to 1mm particle size and stored at room temperature. Compositional analysis showed that, it contains approximately 42.40% glucan and 23.20% xylan (The individual monomer carbohydrate content was determined by the method of LAP # 002 of NREL using HPLC, Zodiac. Ltd). Klason (acid insoluble) lignin was found to be 24.18%, determined by method adopted by Teramoto *et al.*, (2008).

Microorganisms

Saccharomyces cerevisiae MTCC 36 and *Pachysolen tannophilus* MTCC 1077 were procured from Microbial Type Culture Collection, IMTECH-Chandigarh, India and were maintained on Yeast and Malt Extract Agar (YMmedium). The medium was prepared in distilled water by adding 0.3% yeast extract, 0.3% malt extract, 0.5% peptone and 1% glucose, and pH 6.5.

Saccharification and detoxification of cotton stalk

Cotton stalk was subjected to dual stage sulfuric acid treatment. During its first stage 75% H_2SO_4 was used to decrystallize the biomass under specific sample acid ratio of 1:2 (by weight) followed by diluting the same up to 1N in second stage, then employing steam under pressure at 121°C in an autoclave for 30 minutes and four hour heat treatment at 90°C in water bath (Baig,

2014). The obtained acid hydrolysate was detoxified by addition of dried lime up to pH 10 for an hour and then filtered and pH was readjusted up to 6 with acid. This is followed by 4% (w/v) charcoal treatment for half an hour with stirring and then filtered (Baig and Dharmadhikari, 2014). The obtained filtrate solution was used as sole carbon source for fermentation studies.

Inoculum development

Cell mass of *Saccharomyces cerevisiae* and *Pachysolen tannophilus* required for the growth of inoculum was prepared by transferring it aseptically from slants to YM medium. The cells were allowed to grow aerobically in flask at 30°C on rotary shaker incubator with 150 rpm for 48 hours. After incubation, completely activated yeast cell were harvest by centrifugation with 4000 rpm at 4°C for 10 minutes, washed with distilled water and transferred to cotton stalk hydrolysate supplemented with 0.5% yeast extract, 1% peptone and pH was adjusted to 5.5. The flasks were incubated on rotary shaker incubator with 150 rpm at 30°C for 24 hours and grown aerobically to promote healthy growth of yeast cell in hydrolysate. After incubation these activated cells of *Saccharomyces cerevisiae* and *Pachysolen tannophilus* were mixed in the proportion of 60% and 40% respectively. Cells were quantified to ensure the initial inoculation stayed at approximately 6×10^7 cfu/mL corresponding to 10 gram dry weight/liter. Total suspension of yeast cell was centrifuged at 5000 rpm for 5 minute at 4°C and cell pellets were washed with distilled water and stored at 4°C for beads preparation.

Preparation of beads from co culture inoculum of yeast cells

To carry out immobilization, 2% CaCl₂ solution was prepared in an aqueous

medium and kept at 4°C for chilling. Subsequently sodium alginate solution (2% w/v) was prepared in hot water by stirring on magnetic stirrer. Dry pellets (inoculum) of yeast cell which was stored for bead preparation, mixed with sodium alginate solution thoroughly to form homogenous mixture. This homogeneous mixture was extruded slowly drop by drop through stainless steel needle using syringe pump into 2% chilled CaCl₂ solution which form the calcium alginate beads of yeast cell containing co-culture of *Saccharomyces cerevisiae* and *Pachysolen tannophilus*. These beads were aseptically stored at 4°C for further studies.

Ethanol production using immobilized yeast cells

Fermentation was performed in 250 ml of Erlenmeyer flask containing 150 ml of cotton stalk hydrolysate to fulfill the requirement of semi aerobic mode of aeration. All the fermentations were operated in batch manner with a fixed parameter and supplemented with 0.5% yeast extract, 1% peptone, pH 5.5 and temperature of 30°C. The fermentation was initiated with inoculation of calcium alginate beads of *Saccharomyces cerevisiae* and *Pachysolen tannophilus* (corresponds to 10% co culture inoculum) into flasks and sealed with aluminum foil and allowed to ferment on rotary shaker incubator with an agitation rate of 120 rpm. Samples were collected at 12 hours interval throughout the fermentation from individual flask at one time, so as to maintain the ideal environmental condition during fermentation (72 hours), and were subjected to estimation of ethanol and residual sugar simultaneously (Baig, 2014).

Recycling of immobilized yeast cells

In order to examine the recycling potential of immobilized cells, at the end of

fermentation cycle, the calcium alginate beads were retained, washed with sterile saline and transferred to the similar volume of fresh medium for the next cycle of fermentation. The cycles were repeated again and again till change in physiology of beads or productivity of fermentation was observed.

Analytical methods

The DNSA method of Miller, (1959) was adopted to quantify the amount of reducing sugars present in the sample. Glucose oxidase method, for an enzymatic assay of glucose was performed by following the

guideline given by Bregmeyer *et al.*, (1974). Total content of phenolic compound in hydrolysate was determined by Folin-Ciocalteus (FC) method (Singleton and Rossi, 1965). Furans were estimated with spectrophotometric method as described by Martinez *et al.*, (2000). Ethanol estimation was carried out by Gas Chromatography (Shimadzu Japan). GC was carried out according to NREL procedure LAP # 011, using ZB-Wax column (30mm × 0.25mm) with Flame Ionization Detector (FID). Cell density was measured turbidometrically at 600 nm by using UV-VIS spectrophotometer (Srilekha Yadav *et al.*, 2011).

Fermentation efficiency

Fermentation efficiency was calculated as

$$\text{Fermentation efficiency} = \frac{\text{Practical yield of ethanol}}{\text{Theoretical yield of ethanol}} \times 100$$

Theoretical yield is 0.511 gram per gram of sugar consumed.

Results and Discussion

Saccharification and detoxification of cotton stalk

The two stage acid hydrolysis of cotton stalk yielded maximum fermentable sugar and specifically D-glucose of 0.49 g/g and 0.36 g/g of biomass (native cotton stalk) respectively. The byproducts of hydrolysis such as furans and phenolics were also formed with a concentration of 1.971 mg/L and 4.909 g/L respectively (Table.1). To overcome these inhibitors, detoxification with over liming up to pH 10 for an hour followed by filtration and by maintaining pH 6; 4% charcoal treatment for half an hour gives maximum reduction in inhibitors including 92.69% furans and 88.89%

phenolics while 19.84% sugar losses were also reported during process (Baig and Dharmadhikari, 2014). The detoxified hydrolysate achieved having sugar concentration of 11 g/L, corresponds to a yield of 0.396 g/g of biomass; it is then exposed to fermentation for ethanol production.

Fermentation using immobilized co culture

Fermentation was initiated by introducing Ca-alginate beads containing co culture inoculum of *Saccharomyces cerevisiae* and *Pachysolen tannophilus* (which corresponds to 10% inoculum), into flask contains cotton stalk hydrolysate and was incubated at 30°C for 72 hours. The outcomes of all

experiments were analyzed in terms of substrate utilization and product formation and reliability of the results were checked by passing through ANOVA. As the fermentation process started, the data showed that ethanol was not detected in first 6 hours of fermentation, while it commence from 12 hours onwards and reached maximum at 36 hours of fermentation. The concentration of ethanol was started from 0.71 g/L after 12 hours of fermentation and reached to 3.94 g/L at 36 hours of fermentation corresponds to an yield of 0.142 g/g of biomass (native cotton stalk), 0.221 g/g of holocelluloses and 0.355 g/g of fermentable sugar available for yeast cell and during this stage the highest fermentation efficiency was recorded as 69.53%. Meanwhile, the sugar concentration in the medium dropped sharply to more than 90% within 36 hours of fermentation and stayed constant thereafter. These findings

were harmony with the results reported earlier (Wendhausen *et al.*, 2001).

Effect of recycling on ethanol production by immobilized yeast cells

Cycles of repeated batch operations with the immobilized yeast performed, using the same process conditions as in the first batch fermentation, each of them tested for 36 hours. The ethanol concentration was noted as 3.94 g/L, corresponds to yield of 0.142 g/g of native cotton stalk, 0.221 g/g of holocelluloses and 0.355 g/g of fermentable sugars in first batch; and 3.96 g/L corresponds to a yield of 0.143 g/g of native cotton stalk, 0.222 g/g of holocelluloses and 0.356 g/g of fermentable sugars in subsequent batch fermentation respectively. The fermentation efficiencies in first and second cycle were noted as 69.53% and 69.88% respectively.

Table.1 Ethanol fermentation from cotton stalk hydrolysate by using immobilized culture of *Saccharomyces cerevisiae* and *Pachysolen tannophilus*

Time period (hr)	Ethanol conc. (g/L)	Ethanol yield (g/g)			Fermentation efficiency (%)	Sugar consumed (%)
		Biomass	Holocelluloses	Fermentable sugar		
6	00	000	000	000	00	12.70
12	0.71	0.026	0.040	0.064	12.53	26.29
24	2.08	0.075	0.116	0.187	36.71	52.38
36	3.94	0.142	0.221	0.355	69.53	90.18
48	3.92	0.141	0.220	0.353	69.18	90.21
60	3.91	0.141	0.219	0.352	69.00	90.27
72	3.89	0.140	0.218	0.350	68.65	90.29
SEm±	0.16	0.007	0.007	0.0019	00.38	1.72
CD at 5%	0.47	0.021	0.021	0.0060	01.17	5.20

Table.2 Effect of recycling on immobilized culture of *Saccharomyces cerevisiae* and *Pachysolen tannophilus*

Fermentation cycles	Ethanol conc. (g/L)	Ethanol yield (g/g)			Fermentation efficiency (%)	Sugar consumed (%)
		Biomass	Holocelluloses	Fermentable sugar		
First batch	3.94	0.142	0.221	0.355	69.53	90.18
Second batch	3.96	0.143	0.222	0.356	69.88	97.26
Third batch	Destruction of Ca-alginate beads occurred					

Fig.1 Effect of time on ethanol concentration from cotton stalk hydrolysate by immobilized co-culture of *Saccharomyces cerevisiae* and *Pachysolen tannophilus*

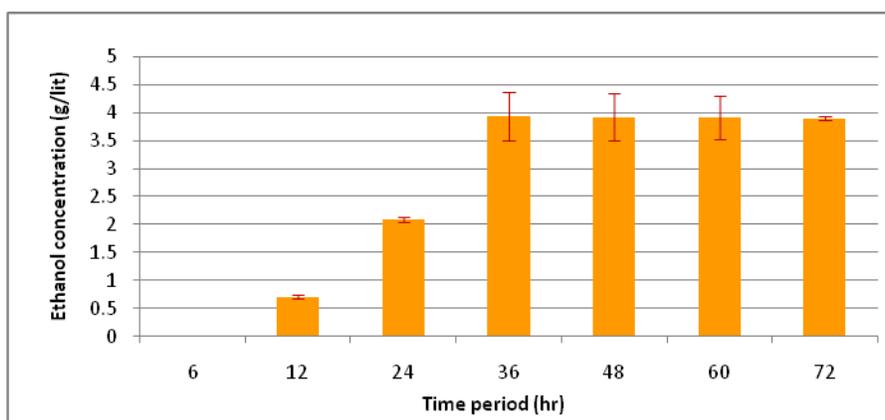


Fig.2 Effect of time on ethanol yield from cotton stalk hydrolysate by immobilized co-culture

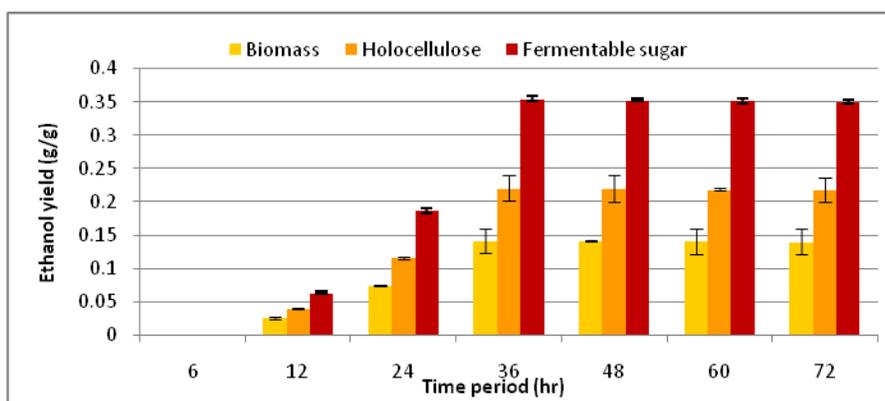
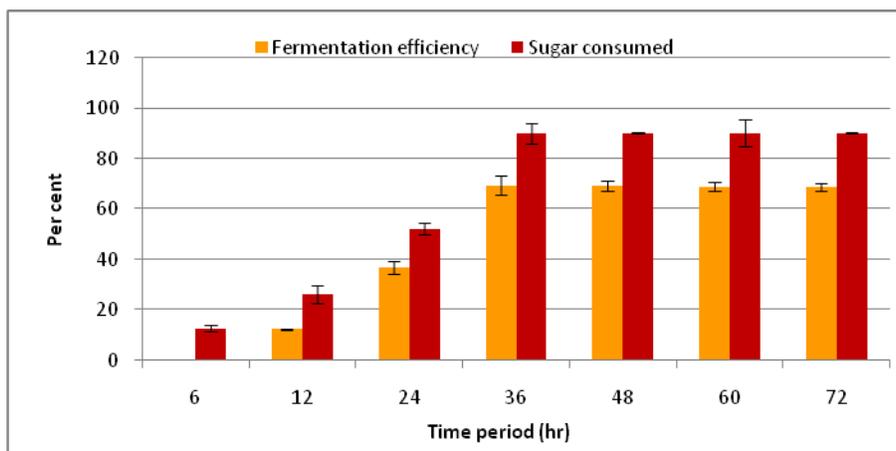


Fig.3 Fermentation efficiency and sugar consumed during ethanol fermentation

The ethanol concentration and ethanol yield remain almost constant during the repeated batch fermentation, as was observed from obtained results shown in Table 2. It was interesting to note that immobilized yeast cell effectively consumed more than 90% sugar in both cycles, while beads dimension was observed slightly increased in subsequent cycles. However, during third cycle of fermentation resulted in destruction of Ca-alginate beads occurred, and this was might be due to intensive growth of cells and CO₂ evolution during the fermentation. The intensive proliferation of yeast cells inside the matrix caused instability of Ca-alginate in acid condition during fermentation, as was reported by Rakin *et al.*, (2009). It was considered that, after repeated cycles the overgrowth of test organisms in the gel beads caused inhibition of substrate diffusion (sugars) inside and the product (ethanol) outside (Aithal, 2001). Bakers *et al.*, (2001) investigated batch fermentation of sucrose using *Zymomonas mobilis* cells immobilized in Ca-alginate and reported that Ca-alginate beads disintegrated after 4-5 days. From one more investigation, it has also been reported that, maximum ethanol production was observed up to 4th cycle in repeated batch fermentation system from glucose as carbon source using

Saccharomyces cerevisiae VS₃ immobilized in calcium alginate beads (Sree *et al.*, 1999). While in present study comparatively less repeated cycles were possible, which might be due to presence of traces of inhibitors even after detoxification. It was observed that, though immobilized cell fermentation is preferred with respect to the advantages of high cell concentration and easy separation of biocatalysts, maintenance of the mechanical structure of the gel matrix usually requires additional attention. Therefore, compared to batch culture, continuous cultivation of the hydrolysate with regular input of the fresh immobilized cells during fermentation is supposed to be better option for ethanol production, as was also recommended by Yang (2008).

In addition to the present study, various carriers may also use in future to make the process more feasible and productive. In this regards, Rakin *et al.*, (2009), investigated the effect of immobilized *Saccharomyces cerevisiae* using Ca-alginate using corn meal hydrolysate for bioethanol production for repeated batch fermentation and found that alginate gels degraded after the second fermentation cycle, while PVA carrier exhibited better mechanical properties and stability, however lower ethanol

concentration were achieved during the fermentation.

In conclusion, a successful attempt has been made to immobilize the cell of *Saccharomyces cerevisiae* and *Pachysolen tannophilus* in calcium alginate matrix and from this; peak ethanol concentration of 3.94 g/L (corresponds to yield of 0.355 g/g of available sugar) was achieved after 36 h of fermentation. Recycling of immobilized cell showed no significant change in concentration, yield and fermentation efficiency were observed in between first two batches, and during third cycle, beads became disintegrated. The present study is limited to laboratory scale only, and sincere efforts are needed to make the process more feasible and economical.

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